

## Research



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# The effect of density changes on crystallization with a mushy layer

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A nonlinear problem with two moving boundaries of the phase transition, which describes the process of directional crystallization in the presence of a quasi-equilibrium two-phase layer, is solved analytically for the steady-state process. The exact analytical solution in a two-phase layer is found in a parametric form (the solid phase fraction plays the role of this parameter) with allowance for possible changes in the density of the liquid phase accordingly to a linearized equation of state and arbitrary value of the solid fraction at the boundary between the two-phase and solid layers. Namely, the solute concentration, temperature, solid fraction in the mushy layer, liquid and solid phases, mushy layer thickness and its velocity are found analytically. The theory under consideration is in good agreement with experimental data. The obtained solutions have great potential applications in analysing similar processes with a two-phase layer met in materials science, geophysics, biophysics and medical physics, where the directional crystallization processes with a quasi-equilibrium mushy layer can occur.

This article is part of the theme issue 'Patterns in soft and biological matters'.

## 1. Introduction

The phase transition processes in the presence of a two-phase solid/liquid layer frequently occur in a large variety of applied problems ranging from solidification in materials science, chemical industry and geophysics (e.g. crystallization of sea ices, lava

lakes and at the Earth's inner core) to crystallization in biophysics and medical physics (e.g. biocrystallization and crystallization of proteins and DNA complexes) [1–13]. A two-phase layer lying between solid and liquid substances is filled with the liquid phase and growing solid structures. This layer moves in the direction of increasing temperature and its time-dependent coordinates and velocity should be found from the solution of the moving boundary problem. The first theoretical models of the two-phase (mushy) layer were developed by Hills, Loper, Roberts, Fowler and Borisov in the 1980s [14–17]. Note that a complete theoretical description of such a process is complicated by the presence of different physical mechanisms such as dendritic growth and nucleation of crystals, buoyancy and gravitational forces, solute impurities, coarsening kinetics, joule heating, convective and hydrodynamic flows etc. (see, among others, [18–32]).

In the present paper, a new analytical approach for solving a nonlinear heat and mass transfer equations in a two-phase layer is developed in the steady-state crystallization conditions with allowance for the temperature- and concentration-dependent density in liquid. This approach extends previously known analytical solutions of mushy layer equations for the steady-state solidification regime [33,34] and enables us to describe a wider class of crystallization problems met in applied science. The theory under consideration can be used for the description of directional solidification processes of binary melts and solutions with a mushy layer in materials science, geophysics, biophysics and medical physics taking into account the temperature- and concentration-dependent density in liquid.

## 2. The model

Let us consider the process of directional solidification along the spatial coordinate  $\xi$  (figure 1). The solid phase/mushy layer phase boundary is  $\Sigma(\tau)$  whereas the mushy layer/liquid phase boundary is  $\Sigma(\tau) + \delta$ , where  $\tau$  and  $\delta$  represent the time and two-phase layer thickness. The solid material, two-phase layer and liquid phase are, respectively, located in regions  $\xi < \Sigma(\tau)$ ,  $\Sigma(\tau) < \xi < \Sigma(\tau) + \delta$  and  $\xi > \Sigma(\tau) + \delta$ . The heat and mass transfer equations in the two-phase layer can be written as (see, among others, [14–16,33–36])

$$\left. \begin{aligned} \rho_m C_m \frac{\partial \theta_m}{\partial \tau} &= \frac{\partial}{\partial \xi} \left( \lambda_m \frac{\partial \theta_m}{\partial \xi} \right) + L_V \frac{\partial \varphi}{\partial \tau} \\ \text{and} \quad \theta_m &= \theta_L(\sigma_0) + \Gamma(\sigma_m - \sigma_0), \quad \Sigma(\tau) < \xi < \Sigma(\tau) + \delta, \end{aligned} \right\} \quad (2.1)$$

$$\frac{\partial}{\partial \tau} [(1 - \varphi)\sigma_m] = \frac{\partial}{\partial \xi} \left( D_m \frac{\partial \sigma_m}{\partial \xi} \right) - k\sigma_m \frac{\partial \varphi}{\partial \tau}, \quad \Sigma(\tau) < \xi < \Sigma(\tau) + \delta, \quad (2.2)$$

where  $\theta_m$  and  $\sigma_m$  are the temperature and solute concentration in the two-phase layer,  $\varphi$  is the fraction of solid phase,  $L_V$  is the latent heat parameter,  $\sigma_0$  is a reference value of the solute concentration in liquid,  $\theta_L$  is the liquidus temperature,  $\Gamma$  is the slope of the liquidus line,  $k$  is the equilibrium segregation coefficient, and the density  $\rho_m$ , heat capacity  $C_m$ , thermal conductivity  $\lambda_m$  and diffusion coefficient  $D_m$  in the two-phase layer can be expressed as volume-fraction-weighted averages of the properties of liquid and solid [37]

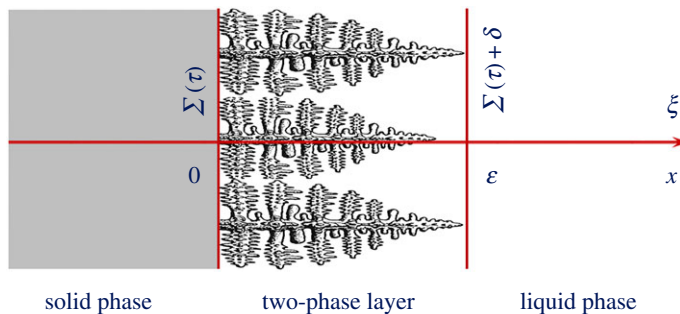
$$\rho_m C_m = \rho_l C_l(1 - \varphi) + \rho_s C_s \varphi, \quad \lambda_m = \lambda_l(1 - \varphi) + \lambda_s \varphi \quad \text{and} \quad D_m = D_l(1 - \varphi), \quad (2.3)$$

where we traditionally neglect diffusion in the solid phase. Here,  $\rho_l$  and  $\rho_s$  are the densities in the liquid and solid phases,  $C_l$  and  $C_s$  are the heat capacities in these phases,  $\lambda_l$  and  $\lambda_s$  are the thermal conductivities in liquid and solid, and  $D_l$  represents the diffusion coefficient in liquid.

The density of the fluid changes accordingly to a linearized equation of state

$$\rho_l = \rho_0 \{1 - \alpha^* [\theta_m - \theta_L(\sigma_0)] + \beta^* (\sigma_m - \sigma_0)\}, \quad (2.4)$$

where  $\rho_0$  is a reference density,  $\alpha^*$  and  $\beta^*$  are the constant expansion coefficients for heat and solute.



**Figure 1.** Schematic illustration of the directional solidification process with a two-phase layer where the growing solid phase in the form of dendrite-like structures is shown. (Online version in colour.)

The boundary conditions at the solid phase/two-phase layer (at  $\xi = \Sigma(\tau)$ ) and two-phase layer/liquid phase (at  $\xi = \Sigma(\tau) + \delta$ ) boundaries have the form [33–36]

$$\left. \begin{aligned} \lambda_s \frac{\partial \theta_s}{\partial \xi} - \lambda_m \frac{\partial \theta_m}{\partial \xi} &= L_V(1 - \varphi_*) \frac{d\Sigma}{d\tau} \\ (1 - k)(1 - \varphi_*)\sigma_m \frac{d\Sigma}{d\tau} + D_m \frac{\partial \sigma_m}{\partial \xi} &= 0, \quad \varphi = \varphi_*, \quad \xi = \Sigma(\tau), \end{aligned} \right\} \quad (2.5)$$

and

$$\sigma_m = \sigma_l, \quad \frac{\partial \sigma_m}{\partial \xi} = \frac{\partial \sigma_l}{\partial \xi}, \quad \frac{\partial \theta_m}{\partial \xi} = \frac{\partial \theta_l}{\partial \xi}, \quad \varphi = 0, \quad \xi = \Sigma(\tau) + \delta, \quad (2.6)$$

where  $\theta_s$  and  $\theta_l$  represent the temperatures in the solid and liquid phases,  $\varphi_*$  is the solid fraction at the solid phase/two-phase layer boundary, and  $\sigma_l$  is the solute concentration in liquid.

We consider the solidification process at fixed temperature gradients. In this case, the temperature and concentration fields in the solid (at  $\xi < \Sigma(\tau)$ ) and liquid (at  $\xi > \Sigma(\tau) + \delta$ ) phases are described by equations

$$\frac{\partial \theta_s}{\partial \xi} = g_s, \quad \xi < \Sigma(\tau); \quad \frac{\partial \theta_l}{\partial \xi} = g_l, \quad \frac{\partial \sigma_l}{\partial \tau} = D_l \frac{\partial^2 \sigma_l}{\partial \xi^2}, \quad \xi > \Sigma(\tau) + \delta; \quad \sigma_l \rightarrow \sigma_0, \quad \xi \rightarrow \infty, \quad (2.7)$$

where  $g_s$  and  $g_l$  represent the constant temperature gradients in the solid and liquid phases and the two-phase layer thickness does not depend on time [31,32,38].

The model (2.1)–(2.7) is the nonlinear model with two moving boundaries of the phase transition. Note that there are no general methods for solving such models. Below we consider how to find the exact analytical solution of equations (2.1)–(2.7) in the case of steady-state solidification with a constant velocity  $d\Sigma/d\tau = u_s$ , which must be determined from the solution of the problem.

### 3. Analytical solution

For the sake of convenience, let us introduce the following dimensionless variables and parameters

$$\left. \begin{aligned} x &= \frac{u_s}{D_l} (\xi - u_s \tau), \quad c_m = \frac{\sigma_m}{\sigma_0}, \quad c_l = \frac{\sigma_l}{\sigma_0}, \quad T_m = \frac{\theta_m}{m\sigma_0}, \quad \Lambda_0(\varphi) = \frac{\lambda_m(\varphi)}{\lambda_s}, \\ \tilde{\beta} &= (\beta^* + m\alpha^*)\sigma_0, \quad R = \frac{\rho_s C_s}{\rho_0 C_l}, \quad m = -\Gamma, \quad T_0 = \frac{\theta_0}{m\sigma_0}, \quad \theta_0 = \theta_L(\sigma_0) - \Gamma\sigma_0, \\ a_1 &= \frac{\lambda_s}{\rho_0 C_l D_l}, \quad a_2 = \frac{L_V}{\rho_0 C_l m \sigma_0}, \quad \tilde{L}_V = \frac{L_V D_l}{\lambda_s m \sigma_0}, \quad G_s = \frac{g_s D_l}{u_s m \sigma_0}, \quad G_l = \frac{g_l D_l}{u_s m \sigma_0} \\ \varepsilon &= \frac{u_s \delta}{D_l}, \quad g(c_m, \varphi) = [1 + \tilde{\beta}(c_m - 1)](1 - \varphi) + R\varphi. \end{aligned} \right\} \quad (3.1)$$

and

The nonlinear model (2.1)–(2.7) in dimensionless variables (3.1) takes the form

$$g(c_m, \varphi) \frac{dc_m}{dx} + a_1 \frac{d}{dx} \left[ \Lambda_0(\varphi) \frac{dc_m}{dx} \right] + a_2 \frac{d\varphi}{dx} = 0, \quad T_m = T_0 - c_m, \quad 0 < x < \varepsilon, \quad (3.2)$$

$$\frac{d}{dx} [(1 - \varphi)c_m] + \frac{d}{dx} \left[ (1 - \varphi) \frac{dc_m}{dx} \right] + kc_m \frac{d\varphi}{dx} = 0, \quad 0 < x < \varepsilon, \quad (3.3)$$

$$G_s + \Lambda_0(\varphi_*) \frac{dc_m}{dx} = \tilde{L}_V(1 - \varphi_*), \quad \varphi = \varphi_*, \quad x = 0, \quad (3.4)$$

$$(1 - k)c_m + \frac{dc_m}{dx} = 0, \quad x = 0 \text{ if } \varphi_* \neq 1, \text{ otherwise } \varphi_* = 1, \quad x = 0, \quad (3.5)$$

$$c_m = c_l, \quad \frac{dc_m}{dx} = \frac{dc_l}{dx} = -G_l, \quad \varphi = 0, \quad x = \varepsilon \quad (3.6)$$

and 
$$\frac{d^2 c_l}{dx^2} + \frac{dc_l}{dx} = 0, \quad x > \varepsilon \text{ and } c_l \rightarrow 1, \quad x \rightarrow \infty. \quad (3.7)$$

After integration of the first equation (3.7), we can easily find the concentration distribution in the liquid phase (at  $x > \varepsilon$ ). Using the third boundary condition (3.6) and the last expression (3.7), we finally obtain

$$c_l(x) = 1 + G_l \exp(\varepsilon - x), \quad x > \varepsilon. \quad (3.8)$$

In order to determine the concentration field in the two-phase layer (at  $0 < x < \varepsilon$ ), let us express the concentration derivative  $dc_m/dx = c_{mx}$  from equations (3.2) and (3.3) as

$$\frac{dc_m}{dx} = c_{mx} = \frac{[f_1(\varphi) - f_2(\varphi)c_m] dc_m/d\varphi - f_3(\varphi) - f_4(\varphi)c_m}{f_5(\varphi)}, \quad 0 < x < \varepsilon, \quad (3.9)$$

where

$$f_1(\varphi) = (1 - \varphi) \left[ a_1 \Lambda_0(\varphi) + (\tilde{\beta} - 1)(1 - \varphi) - R\varphi \right], \quad f_2(\varphi) = \tilde{\beta}(1 - \varphi)^2,$$

and

$$f_3(\varphi) = a_2(1 - \varphi), \quad f_4(\varphi) = (1 - k)a_1 \Lambda_0(\varphi), \quad f_5(\varphi) = a_1 \left[ (1 - \varphi) \frac{d\Lambda_0}{d\varphi} + \Lambda_0(\varphi) \right].$$

Now substituting  $dc_m/dx$  from (3.9) into equation (3.3), we come to the following Cauchy problem for concentration  $c_m$  as a function of  $\varphi$  in the two-phase layer ( $c'_m = dc_m/d\varphi$ ,  $df_5/d\varphi = 0$ )

$$\frac{d^2 c_m}{d\varphi^2} = \frac{F(c'_m, c_m, \varphi)f_5(\varphi) - (1 - \varphi)h_1(c'_m, c_m, \varphi)}{(1 - \varphi)h_2(c_m, \varphi)} \quad (3.10)$$

and

$$c_m = 1 + G_l, \text{ and } \frac{dc_m}{d\varphi} = \frac{f_3(0) + (1 + G_l)f_4(0) - G_l f_5(0)}{f_1(0) - (1 + G_l)f_2(0)}, \quad \varphi = 0, \quad (3.11)$$

where

$$h_1(c'_m, c_m, \varphi) = [f'_1(\varphi) - f'_2(\varphi)c_m - f_2(\varphi)c'_m]c'_m - f'_3(\varphi) - f'_4(\varphi)c_m - f_4(\varphi)c'_m$$

and

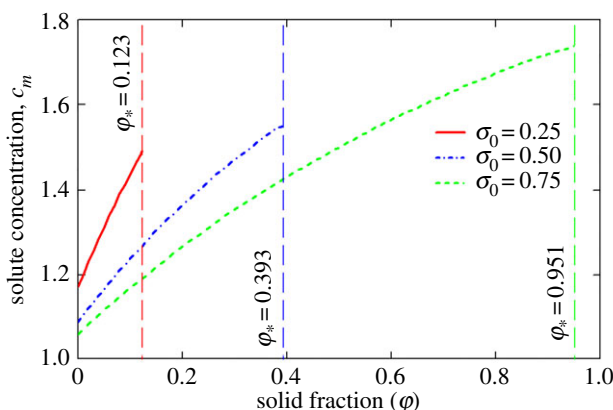
$$h_2(c_m, \varphi) = f_1(\varphi) - f_2(\varphi)c_m, \quad F(c'_m, c_m, \varphi) = (1 - k)c_m - (1 - \varphi)c'_m + c_{mx}(c'_m, c_m, \varphi),$$

and expressions (3.6), (3.8) and (3.9) have been used.

If  $\varphi_* \neq 1$ , one can determine the following expression for  $\varphi_*$  from the boundary conditions (3.4) and (3.5)

$$c_m(\varphi_*) = \frac{G_s - \tilde{L}_V(1 - \varphi_*)}{(1 - k)\Lambda_0(\varphi_*)}, \quad (3.12)$$

where  $c_m(\varphi_*)$  must be found from the solution of Cauchy problem (3.10), (3.11). The first expression (3.5) in this case defines  $u_s$  from the equation  $(1 - k)c_m(\varphi_*) + c_{mx}(\varphi_*) = 0$ , where  $c_{mx}$  is determined in (3.9). In the opposite case, when  $\varphi_* = 1$ , the boundary condition (3.4) determines the steady-state velocity  $u_s$ .



**Figure 2.** The solute concentration as a function of the solid fraction in the two-phase layer. The vertical lines show the solid phase/two-phase layer boundary where  $\varphi = \varphi_*$ . Parameters used for calculations (Fe–Ni alloy) are  $\lambda_l/\lambda_s = 0.565$ ,  $\tilde{\beta} = 0.75$ ,  $\tilde{L}_V = 0.538$ ,  $R = 0.623$ ,  $k = 0.68$ ,  $a_1 = 4958$ ,  $a_2 = 2.669$ ,  $G_l = 0.057$  and  $G_s = 0.57$ . (Online version in colour.)

Now taking into account that  $dc_m/dx = (dc_m/d\varphi)(d\varphi/dx)$ , we arrive at the following explicit solutions for the dimensionless thickness of two-phase layer  $\varepsilon$  and  $x(\varphi)$

$$\varepsilon = - \int_0^{\varphi_*} \frac{dc_m/d\varphi_1}{c_{mx}(\varphi_1)} d\varphi_1 \quad \text{and} \quad x(\varphi) = \varepsilon + \int_0^{\varphi} \frac{dc_m/d\varphi_1}{c_{mx}(\varphi_1)} d\varphi_1, \quad (3.13)$$

where again  $c_{mx}(\varphi_1)$  and  $dc_m/d\varphi_1$  are determined by expressions (3.9)–(3.11).

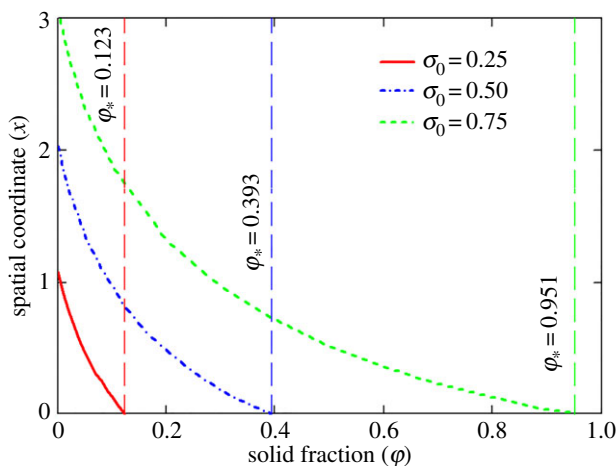
Thus, a complete analytical solution in the two-phase layer, (3.9)–(3.13), is found in a parametric form (with parameter  $\varphi$ ).

## 4. Conclusion

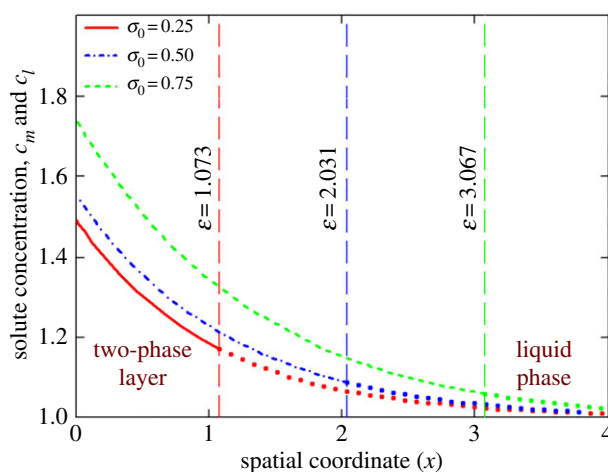
The obtained analytical solution for the solute concentration in the two-phase and liquid layers is illustrated in figures 2–4. Note that the temperature field in the mixed layer is also determined in accordance with the second expression (3.2) whereas in the solid and liquid layers it is defined by the constant temperature gradients (see equations (2.7)). Figures 2 and 3 show the solute concentration  $c_m$  and spatial coordinate  $x$  as functions of the solid fraction  $\varphi$  accordingly to exact analytical solutions (3.10), (3.11) and (3.13). Let us emphasize that the solute concentration increases with increasing  $\varphi$  (decreasing  $x$ ), i.e.  $c_m$  attains its maximum at the boundary between the solid and two-phase layers (at  $\varphi = \varphi_*$ ).

The parametric solutions  $c_m(\varphi)$  and  $x(\varphi)$  in the two-phase layer enable us to find the solute concentration  $c_m$  as a function of the spatial coordinate  $x$ . This dependence is shown in figure 4 on the left-hand side of the corresponding vertical line plotted for a certain initial concentration  $\sigma_0$ . The concentration  $c_l$  in the liquid region shown in figure 4 by the dotted lines on the right-hand side of each vertical line is demonstrated accordingly to expression (3.8). Note that the concentration profiles  $c_m(x)$  and  $c_l(x)$  coincide at the two-phase layer/liquid phase boundary and determine the thickness  $\varepsilon$  of the two-phase region. The greater values of initial concentration  $\sigma_0$  increase the two-phase layer thickness  $\varepsilon$  and the solid fraction  $\varphi_*$  at the solid phase/two-phase layer boundary. The interfacial concentration  $\sigma_s = k\sigma_0 c_m$  determined on the left-hand side of the boundary solid phase/two-phase layer enables us to obtain the concentration distribution in the solid phase appearing as a result of impurity absorption by the solid phase at  $x = 0$ . Thus, the obtained solutions completely describe the concentration and temperature profiles, the solid phase distribution as well as the steady-state velocity of the two-phase layer and its thickness.

Figure 5 compares the impurity concentration in the solid phase calculated accordingly to the theory under consideration and experimental data [39] for a set of KCl crystals. It is easily seen that the theory well agrees with experiments. An important point is that the present analytical



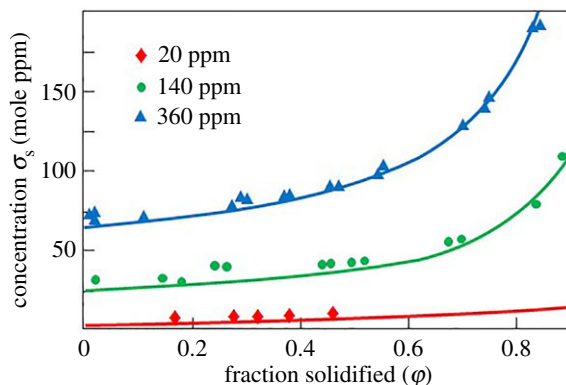
**Figure 3.** The spatial coordinate as a function of the solid fraction in the two-phase layer. The vertical lines show the solid phase/two-phase layer boundary where  $\varphi = \varphi_*$  and  $x = 0$ . (Online version in colour.)



**Figure 4.** The solute concentration as a function of the spatial coordinate in the two-phase and liquid layers. The vertical lines show the boundary between the two-phase and liquid layers. The profile of solute concentration  $c_l$  in the liquid layer (dots) lies on the right-hand side of the vertical line plotted for a certain concentration  $\sigma_0$ . (Online version in colour.)

solution transforms to the previously known steady-state solutions [33,34] in the limiting case of constant density in the liquid phase, i.e. if  $\alpha^* = \beta^* = 0$ , and  $\rho_l = \rho_0 = \text{const}$ .

In summary, the theory under consideration shows how to construct an exact analytical solution of nonlinear phase transition problem in the presence of a mixed layer where the solid and liquid phases coexist together and their fractions must be determined from the solution of the moving boundary problem. Note that the general methods for solving such nonlinear heat and mass transfer problems with two moving boundaries are unknown. Within the framework of the formulated heat and mass transfer equations, the developed theory contains no limitations and can be applied to the description of various processes of steady-state crystallization. The theory takes into account possible variations of the density of the liquid phase accordingly to a linearized equation of state and arbitrary value of the solid phase fraction at the boundary between the two-phase and solid layers. The present analytical approach can be used for solving similar problems arising in geophysics, biophysics, medical physics and materials science, where a quasi-equilibrium crystallization with a mushy layer can occur.



**Figure 5.** Theoretical predictions (solid lines) and experimental data [39] (symbols) for a set of KCl crystals doped with  $c_0 = 20$ , 140 and 360 mole ppm of divalent europium,  $c_0 = \sigma_0(1 + G_i)$ ,  $k = 0.18$ ,  $\alpha^* = 0$  and  $\beta^* = 0$ . (Online version in colour.)

Let us especially note in conclusion that the present analysis can be extended to the case of weakly non-equilibrium mushy layer crystallization (where nucleation and growth of crystals occur in a metastable liquid) in the spirit of previously developed theories [40,41]. A step forward for future research will also be the development of a theory of non-stationary crystallization with a two-phase zone, taking into account the temperature and concentration dependence of the density of the liquid phase, by analogy with the previous theories [42,43].

**Data accessibility.** This article does not contain any additional data.

**Authors' contributions.** All authors contributed equally to this study.

**Competing interests.** We declare we have no competing interests.

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